



APPLICATION NOTE



EFFECTIVE REMOVAL OF mAb AGGREGATE USING Ca**Pure-HA® MEDIA WITH POTASSIUM SALTS

INTRODUCTION

Downstream process chromatography scientists are constantly seeking for better and more selective ways to remove aggregates and other process related impurities from a monoclonal antibody (mAb) monomer. Making use of chromatography resins with better selectivity, resolution and capacity is one approach to solving the problem of aggregate removal in monoclonal antibody production.

Ca⁺⁺Pure-HA (hydroxyapatite: Ca (PO₄) (OH)) is a form of calcium phosphate used in the chromatographic separation of biomolecules. Unlike other resins available from Tosoh Bioscience, Ca⁺⁺Pure-HA is both the ligand and the base bead. Hydroxyapatite has unique separation properties for biomolecules and Ca⁺⁺Pure-HA offers unparalleled selectivity and resolution for process scale operations. Its highly selective nature often separates proteins otherwise shown to be homogeneous by electrophoresis and other chromatographic techniques.

Ca⁺⁺Pure-HA is a spherical, macroporous form of the hexagonal crystalline structure of hydroxyapatite. It has been sintered at high temperatures for increased mechanical and chemical stability, allowing it to withstand the rigors of industrial-scale applications. Table 1 lists the properties of Ca⁺⁺Pure-HA.

The data presented here demonstrates the capabilities of Ca⁺⁺Pure-HA media operated with potassium salts such as potassium phosphate and potassium chloride, to remove dimer and higher order aggregates from the monomer of a protein A purified IgG, monoclonal antibody.

PROPERTIES OF Ca++Pure-HA

Table 1

	Ca**Pure-HA
Particle size (mean):	39 µm
Shipped as:	dry powder
pH stability:	6.5 – 14
Shelf life (estimated):	10 years

EXPERIMENTAL CONDITIONS/RESULTS

Purification of IgG₁ using TOYOPEARL AF-rProtein A HC-650F Resin

A crude sample containing IgG_1 was passed through a protein A column and fractions of IgG_1 were collected for further work (Figure 1). The eluate peak was collected and further analyzed by size exclusion chromatography using a TSKgel® G3000SWxL SEC column for monomer and aggregate yield, host cell protein (HCP) content and protein A ligand leaching (see Table 2).

ANALYSIS DATA FOR THE COLLECTED IgG, ELUATE PEAK

PURIFICATION OF $\lg G_{_1}$ FROM CHO SUPERNATANT CRUDE SAMPLE USING TOYOPEARL AF-RPROTEIN A HC-650F RESIN

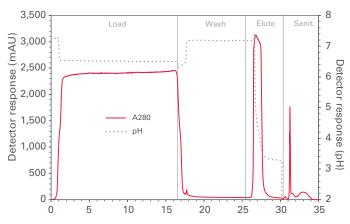


Figure 1

Resin: TOYOPEARL AF-rProtein A HC-650F Column: 25 mm ID × 15 cm (74 mL)

Mobile phase: A: 20 mmol/L Tris-acetate, 150 mmol/L NaCl, pH 7.4

B: 50 mmol/L acetic acid C: 0.1 mol/L NaOH

Flow rate: 225 cm/hr (4 min residence time)
Detection: UV @ 280 nm (mAU), pH

Temperature: ambient

Injection vol.: 1200 mL (48 mg/mL-resin load ratio)
Sample: TBL-mAb-01 CSS @ 2.95 q/L

Instrument: ÄKTA® avant 25

	Protein A Eluate Analysis		
Yield (total IgG)	99%		
Aggregate	4.4% (0.5% HMW, 3.9% dimer)		
НСР	1260 ppm		
Protein A	1.2 ppm		
Table 2			

Removal of mAb aggregates using Ca**Pure-HA media

To remove mAb aggregates from a post-protein A purified sample, Ca**Pure-HA media was used in a polishing chromatography step. The below protocol was used.

Column: $5 \text{ mm ID} \times 5 \text{ cm } (1.0 \text{ mL})$

Mobile phase: A: 50 mmol/L HEPES, 5 mmol/L KPO₄,

pH as indicated

B: mobile phase A + 2.0 mol/L potassium

chloride, pH as indicated

C: 500 mmol/L KPO4, pH as indicated

D: 1.0 mol/L KOH

Gradient: 69.4% B (chloride), 10 CV

gradient delay, 5 CV

Flow rate: 300 cm/hr (1 min residence time)

Detection: UV @ 280 nm (mAU),

Conductivity (mS/cm), pH

Temperature: ambient Injection vol.: 5 µL

Sample: 2.0mg/mL-mediapartially-purifiedmAb-01

(0.2 mL injection)

Instrument: ÄKTA avant 25

Method: Pre-equilibrate, mobile phase C, 3 CV

Equilibrate, mobile phase A, 10 CV

Load

Wash, mobile phase A, 5 CV

Elution, gradient as indicated, 25 CV

Strip, mobile phase C, 5 CV Sanitize, mobile phase D, 5 CV

Data from Figure 2 shows a high resolution separation between the monomer peak and the aggregate peak across three different pH conditions. The elution of the monomer peak at pH 6.5 was delayed and broader.

Figure 3 shows a size exclusion chromatography analysis

REMOVAL OF mAb AGGREGATES FROM THE POST-PROTEIN A PURIFICATION SAMPLE USING CA**PURE-HA MEDIA

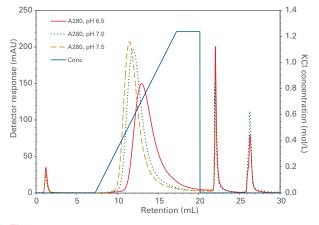


Figure 2

of pooled monomer samples from Figure 2 for the analysis of aggregate content. These samples were injected onto a TSKgel G3000SWxL column. Data analysis show that after the sample passed through Ca⁺⁺Pure HA media under potassium phosphate buffer and potassium chloride operating conditions, mAb aggregates were reduced significantly. In fact, at pH 6.5 operating conditions, the aggregate amount was reduced from 6.6% to as low as 1.3% (Table 3).

AGGREGATE ANALYSIS OF POOLED mAb MONOMER PEAKS ELUTED FROM DIFFERENT PH BUFFERS USING SIZE EXCLUSION

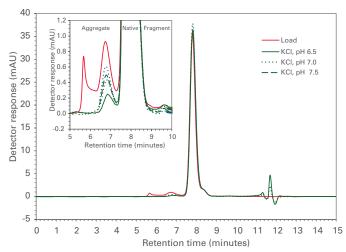


Figure 3

Column: TSKgel G3000SWxL, 7.8 mm ID × 30 cm Mobile phase: 0.1 mol/L phosphate, 0.1 mol/L Na₂SO₄,

0.3% sodium azide, pH 6.7

Flow rate: 1.0 mL/min
Gradient: isocratic
Detection: UV @ 280 nm
Temperature: 25 °C
Injection: 10 µg native

Instrument: HPLC (400 bar pressure)

Salt	рН	Peak molarity (mmol/L)	Recovery (% native)	Aggregate (%)	Fragment (%)
		Load		6.6	0.6
KCI	6.5	814	72.9	1.3	0.5
	7.0	615	80.0	1.8	0.3
	7.5	509	81.0	2.2	0.3

CONCLUSIONS

Table 3

Ca++Pure-HA media is effective for the removal of dimer and higher order aggregates from a purified mAb sample, post-protein A purification step. In fact, when Ca++Pure-HA media was operated using potassium phosphate buffer as a loading buffer and potassium chloride as an elution buffer, the aggregate content was reduced from 6.6% to as low as 1.3%.